

Experimental Study of Non-metallic Inclusions Behaviour in the Tundish during Continuous Casting of Steel

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スウェーデン王立工科大学 Pär G. Jönsson教授による序文

同和訳

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I hereby submit our manuscript entitled "Experimental Study of Non-metallic Inclusions Behaviour in the Tundish during Continuous Casting of Steel" by Jennie K.S. Svensson, Erik Roos, Anders Lagerstedt, Andrey Karasev, Voicu Brabie, and Pär G. Jönsson, for your journal <i>Sanyo Technical Report</i> .
Recently, with an advance of industrial technology, engineering steels are subject to severer use conditions than before. Research projects to decrease non-metallic inclusions in steel are in increasing demands because inclusions may be fracture origins and degrade reliability of steel products. One of our studies will be introduced in this paper regarding high-cleanliness steel production.
This study highlights the behaviour of non-metallic inclusions in a process of continuous casting. We investigated the non-metallic inclusions detected in the process and found that they can be classified into four groups. These origins are discussed by associating their compositions with those of molten steel, tundish slag, and tundish refractory.
We believe that this paper will be of great interest to your readers.
Sincerely yours,
and the second

YAM JONSSAM Professor Pär G. Jönsson

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山陽特殊製鋼技報編集委員 殿	
私はここに、Jennie K.S. Svensson, Erik Roos, And Lagerstedt, Andrey Karasev, Voicu Brabie and Pär Jönsson による論文「連続鋳造中タンディッシュ内にま る非金属介在物の挙動に関する実験研究」を、山陽特 製鋼技報に投稿します。	ers G. け 殊
近年、産業の高度化に伴い、機械部品用鋼の使用環 は過酷化してきています。鋼中の非金属介在物は、破 起点になる可能性があり鉄鋼製品の信頼性を低下させ ことから、介在物低減に関する研究はますます重要にな ています。本論文では、高清浄度鋼の製造に関する我 の研究の一つを紹介します。	境壊るっ々
本研究では、連続鋳造プロセスにおける非金属介在 の挙動に焦点を当てています。本プロセス中に検出さ た介在物を調査し、4つのグループに分類されることを 出しました。これら介在物組成と、溶鋼、タンディッシ スラグおよびタンディッシュ耐火物の組成との関連性を に、介在物の起源について議論を行いました。	物れ見ユ基
本論文は貴誌の読者にとって興味ある内容であると じております。	信
Professor Pär G. Jönsson	
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The tundish has been experimentally mapped to study reactions between the molten steel and the cover powder as well as between the steel and the tundish lining. Steel samples were collected before casting, in the tundish during the casting process, and after casting. During sampling in the tundish the MISS sampler was used in order to make an in-depth study of two parallel positions of the steel/slag and steel/refractory interfaces. Thereafter, the samples were analysed with SEM in combination with EDS to determine the size and compositions of inclusions. The inclusion data were mapped in ternary phase diagrams to determine the origin of the inclusions. The results showed that two main inclusions groups, slag and deoxidation products, could be found in the samples. In addition, the samples contained inclusions that had been formed due to interactions with the refractory lining material.

Key words

tundish; clean steel; continuous casting; industrial plant trials; slag/steel interface; refractory/steel interface; nonmetallic inclusions

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1. Introduction

As the demands with respect to the product quality increase it becomes necessary to improve the steel cleanness and the resulting material properties ^[1,2]. The tundish is final process step in the steelmaking process before casting, where the steel cleanliness may be influenced. In the tundish, alloys can be added, the superheat may be controlled, and the steel melt can be thermally homogenized ^[3]. It is also the last process step before casting where non-metallic inclusions can be removed from the steel phase to the slag phase ^[3-5]. The steel cleanness can also be improved by prevention of reoxidation of the steel melt ^[4-5].

It is known that an inefficient separation of nonmetallic inclusions from the steel to the slag results in an entrapment of inclusions and a poor slab quality ^[6]. If the separation is inefficient, the non-metallic inclusions can accumulate and cause clogging of the submerged entry nozzle (SEN) during teeming. This, in turn, disturbs the casting process ^[7]. Specifically, the composition of these accumulations has been found to be connected with the composition of the non-metallic inclusions in the molten steel in the tundish ^[8].

In the steel-slag-inclusion system in the tundish, the interfacial phenomena control the separation of nonmetallic inclusions from the steel to the slag [4]. This phenomenon is influenced by the dynamic motion of an inclusion across the interface, the slag viscosity and the wettability [9]. The inclusions separations from the steel to the slag is a complex process due to irregularities in density, turbulent fluctuations, reactions and the corresponding element transfer between the steel and the tundish powder/refractory lining ^[10,11]. When the inclusion reaches the slag/metal interface it can: i) pass and be separated to the slag immediately; ii) remain at the interface and agglomerate with other inclusions that can be washed back into the steel bath; and iii) oscillate underneath the interface and can then follow the steel flow back into the steel resulting in product defects [4]. Also, when an inclusion passes the interface and is separated to the slag a steel film can be formed around the inclusion, when the inclusions are about 150-180 µm in diameter [4,12].

Sometimes the inclusions are trapped at a steel/slag interface for some time before they are separated to the slag, due to the instability and turbulence fluctuations at the interface [10,11]. In addition, small inclusions can agglomerate to form bigger inclusions due to the turbulent steel flow and become easier to separate ^[5]. However, the applomeration of nonmetallic inclusions has been found to be improved when the inclusions are in the slag compared to when they are present at the steel/slag interface [13]. In order to get the most favourable separation of inclusions to the slag, it is important with an overall positive wettability (at the molten steel/slag/inclusion interface) as well as a low slag viscosity but still high enough to withstand a slag entrainment into the steel [4,12]. However, it is known that the slag pick-up of Al₂O₃ inclusions in the tundish changes the composition in the slag, which can alter the slag viscosity [14]. The slag in the tundish can also be contaminated by the carryover calcium-aluminate slag from the ladle [15]. The tundish slag layer can also be engulfed by the molten steel in the tundish and thus form new inclusions [10,11]. More specifically, even at low and horizontal velocities slag particles can be torn off from the slag layer and be dispersed into the molten steel ^[11]. Also, the fluid flow pattern of the tundish has shown that a recirculation of the molten steel is responsible for most of the entrainment of the steel into the slag as well as the vice versa dispersion [16]. It has also been reported that the fluid flow will drive away a considerable amount of smaller inclusions inwards and downwards into the tundish, which will prevent a separation of those inclusions from the steel to the slag [16].

The molten steel can get reoxidized by an oxygen pick-up from the atmosphere as well as by the tundish slag or tundish refractories, which can affect the steel cleanness in the final product ^[2,10,17]. The tundish refractory material is a MgO-based refractory that consists of Olivine which is a solid solution of fayalite (Fe₂SiO₄) and forsterite (Mg₂SiO₄) ^[17]. The MgO-based refractory has been proven to be a stable material, due to its reduced content of easily reducible oxides ^[17]. However, olivine can react with aluminium-deoxidized steels according to the following reactions (1) - (6) ^[17]:

 $2Fe + 2O + SiO_2 = Fe_2SiO_4 \tag{1}$

$$\Delta G^{0}_{f} = 1379.93 \text{ [kJ/mole]} (298.15 \text{ K})^{[18]}$$
 (2)

 $Mg_2SiO_4 + SiO_2 = 2MgSiO_3$ (3)

$$\Delta G^{0}_{f} = 3301.44 \ [kJ/mole] \ (298.15 \ K)^{[18]}$$
(4)

 $MgO + Al_2O_3 = MgAl_2O_4$ (5)

$$\Delta G^{0}_{f} = -2188.96 \, [kJ/mole] \, (298.15 \, K)^{[18]}$$
(6)

As the steel penetrate into the refractory lining, spinel particles are formed at the steel/refractory interface, which originate from aluminium from the molten steel ^[1]. At the same time, particles can detach from the refractory and end up in the steel phase near the steel/refractory interface [1,17]. These particles commonly contain silicate-based phases and MgO crystals ^[1]. Due to a large difference in the oxygen potential between the refractory material and the molten steel high oxygen potentials exist, which results in a formation of an oxidised steel layer at the steel/ refractory interface [1]. Air which is trapped in pores and easily reducible oxides present in the refractory material are sources of oxygen [1]. The silicate-based phase can then dissolve all the oxides in the oxidised steel layer at the steel/refractory interface [1]. Thus, liquid complex slags such as Al₂O₃, CaO, FeO, MgO and SiO_2 can be formed ^[1].

Both the tundish refractory lining and the slag can be potential sources or modifiers of the non-metallic inclusion content in the steel ^[2,10]. Therefore, it is important to understand the possible reactions that can take place between the tundish refractory lining and the steel as well as between the steel and slag, in order to produce clean steels ^[4]. Due to the differences between the physical and mathematical models and the full scale system, it is difficult to accurately model the separation of inclusions from the steel to the slag ^[3].

The current study of the inclusion behaviour in the tundish is experimental and it has been carried out in the industry. More specifically, samples of the steel/ slag interface have been collected at two parallel positions as well as at different times in order to study the behaviour of different non-metallic inclusions in the tundish. The focus has been on the steel/slag interface and the steel/refractory interface and to

study how reactions have influenced the size and composition of these inclusions.

2. Experimental

2.1. Sampling of the Slag/Steel Interface

Industrial plant trials were performed at SSAB Special Steels, which is an integrated ore-based plant in Oxelösund, Sweden. The company produces a wide range of structural high-strength steels, with varying applications for lightweight solutions as well as for heavy and demanding applications. The steel route at SSAB is the following: a blast furnace to produce iron, a torpedo to remove sulfur from the iron, a converter to remove carbon and to convert the iron into steel, ladle refining to alloy the steel as well as to control the amounts of hydrogen, sulfur and oxygen, and finally slab casting.

During the industrial trials, a structural steel (0.165% C, 0.055% AI, 1.25% Mn, 0.22% Si, 0.6% Mo, 0.2 % Cr, wt-%) was studied. The ladle treatment took place in a 190 ton ladle, where aluminum was used for deoxidation and calcium was used for a modification of inclusions. After the ladle treatment, the ladle was transported to the casting machine and the casting was done via a tundish with a capacity of 30 tonnes. The steel was used to cast slabs with the dimension of 220x1680 mm. The compositions of the tundish lining material, the cover powder and the bulk powder are presented in **Table 1**.

Table 1. Chemical composition of the materials used in
tundish during casting, wt-%

Component	MgO	CaO	Al ₂ O ₃	SiO ₂	С	Fe ₂ O ₃
Tundish lining	60.0- 65.0	< 2.0	< 2.0	23.0- 28.0	2.0- 3.0	5.0- 7.0
Tundish cover powder*	9	31	11	22	7	1
Bulk cover powder	35	55	1.3	5	0.05	

*Rest of content is loss on ignition

To verify the interaction between slag and molten steel the Momentary Interfacial Solidification Sampling (MISS) sampler ^[10,19] was used. The MISS-sampler is made up of 12 mm thick steel plates, which are welded together as a mould (120×100 mm) with an 80×8 mm column. In **Figure 1a**, the collected sample is presented and it is also marked where the analyzed sample was cut out. Furthermore, the MISS-sampler was insulated with super wool so that the sample would not be heated and the inside of the sample was etched to achieve good wetting conditions. The MISSsamples were collected from the slag/steel interface in the surface region in the tundish. By using the MISSsampler, a sample plate representing the steel/slag interface was obtained ^[11], which later could be studied by using an Field Emission Gun Scanning Electron Microscope (FEG-SEM) , (Zeiss Merlin equipped with Oxford Instruments INCA Feature for Windows 7) combined with an Energy Dispersive Spectrometer (EDS) , X-MAX 50 mm².



Figure 1. The experimental sampling in the tundish: (a) the MISS sample after removal from the sampler with markings of where the analyzed sample was cut out; (b) the MISS samples were collected in the tundish in position 1 and then in position 2.

For each heat, 6 MISS-samplers were used and then reused in the next trial. Totally, three heats were performed. During teeming of the first casting sequence, the samples were collected from the tundish in the beginning of teeming (samples MA1 and MA2), after teeming of approximately half the ladle (samples MB1 and MB2) and at the end of teeming before changing to the next ladle (samples MC1 and MC2). The MISS-sampler was lowered into the tundish and held in the bath for 5 seconds. Two parallel sampling positions were chosen, which easily could be accessed in the tundish, to compare interactions in depth in the tundish. Sampling position 1 was chosen close to the wall (\sim 110-150 mm from the tundish wall) to study if particles from the refractory lining could be found. Sampling position 2 was chosen far away from the refractory wall near the center to study mainly the interactions between the tundish powder and the steel.

The two sampling positions from the melt in the tundish can be seen in **Figure 1b**. Besides the sampling in the tundish, one steel sample (lollipop, 12 mm thickness) per heat was also taken from the liquid steel in the ladle at the Vacuum Degassing Station (VDS) before the casting. Also, one sample was collected from the slab. The analyzed slab sample was collected from one quarter depth from the surface, in the slab plate. In order for the sample to represent the inner quality for steady state, the slab plate was collected after casting of half of the total ladle weight.

2.2. Analysis of Samples from the Tundish

From the MISS-samples, one sample was cut out from the top of the middle part (zone 1 in Figure 1a). All samples were cut into 20×30 mm pieces, pressed into bakelite, ground, polished, and washed by hand. The non-metallic inclusions composition, morphology and Equivalent Circle Diameter (ECD) were determined using a FEG-SEM by using the INCA Feature software in combination with EDS. The INCA Feature study was set to detect inclusions with an ECD value lager than 5.7 µm. Thereafter, each inclusion was manually studied to eliminate errors, i.e. pores or dust. In addition, the samples from the VDS and from the slab were also analysed using INCA Feature in combination with EDS. Finally, the steel composition of all samples was analysed with optical emission spectrometry (OES).

The obtained data from the INCA Feature studies were divided into two groups of non-metallic inclusions; DM inclusions (ECD 5.7-11.2 μ m) and DL inclusions (ECD \geq 11.3 μ m).

3. Results & Discussion

In previous research using the MISS-sampler a slightly convex slag surface was obtained at the top part of the samples ^[11]. In this study, a 2-layer concept with a reactive slag and an insulating layer was used at the

steel plant. The insulating layer is not supposed to melt, but the second layer should melt and form a liquid slag. However, the slag layer formed by the reactive slag was difficult to observe in the MISS samples. Therefore, the focus of the microscopy studies was directed towards studying the inclusions closest to the slag/steel interface in the MISS samples.

The data from the INCA Feature study was normalised with respect to the oxides Al_2O_3 , CaO and MgO, based on the chemical composition of the analysed inclusions. More specifically, the data was normalised due to that the amount of these elements was significantly higher compared to the amounts of the other elements. The ternary phase diagram of the system Al_2O_3 -CaO-MgO is presented in **Figure 2** ^[20]. The data was plotted for each heat and for each sampling time as follows: (a) - after VDS; (b) - in the beginning of casting; (c) - in the middle of the





Figure 2. The ternary phase diagram of the Al₂O₃-CaO-MgO system ^[20].

casting; (d) - at the end of the casting; (e) - slab. In **Figures 3-4**, the ternary phase diagrams show the normalized compositions of the inclusions for heats 2 and 3. The results in heat 3 are similar to the result in heat 1. Therefore, these results are presented for one heat. It can be seen that the inclusions shown in the ternary phase diagrams include inclusions that



- Figure 3. The chemical composition of the inclusions collected during heat 2. The ternary phase diagrams show inclusions from: (a) ladle; (b) the first MISS-A sample from the tundish; (c) the second MISS-B sample from the tundish; (d) the last MISS-C sample from the tundish; (e) the slab after casting.
- Figure 4. The chemical composition of the inclusions collected during heat 3. The ternary phase diagrams show inclusions from: (a) ladle; (b) the first MISS-A sample from the tundish; (c) the second MISS-B sample from the tundish; (d) the last MISS-C sample from the tundish; (e) the slab after casting.

originate from three groups, namely the slag (I) , deoxidation products (II) , and refractory (III) . Inclusions originating from the slag are found in the liquid region, where the casting temperatures were between 1522-1541°C. Aluminium that reacts with O_2 will form Al_2O_3 inclusions. The non-metallic inclusions originating from the deoxidation products have a high Al_2O_3 content of around 60-100 wt-%. The third group of inclusions has a high MgO content and originates from the tundish refractory lining material.

In Table 2, the calculated ladle slag composition used during the vacuum treatment for each heat is presented. The slag composition is close to the liquid zone as are shown in the ternary phase diagram (Figure 2). The inclusions originating from the slag are in the liquid region in the ternary diagram and have low MgO contents, namely <10 wt-%. In the samples from the slab, these types of inclusions are the most dominating types in all heats. Specifically, these inclusions are found in DM and DL sizes of the inclusions in all heats. However, these inclusions are most common for heats 1 and 3. For heat 2 the CaO content is generally <40 wt-% compared to the other heats 1 and 3, where the CaO content is around 40-60 wt-%. The differences can be seen in Tables 3-5. In heat 2, the steel composition has half the Ca content (0.0005 wt-%) compared to the other two heats for samples collected at time B. This correlates well to the overall tendency that a low CaO content in the inclusions (see Figure 3) corresponds to a low Ca content in the molten steel (see Table 4) . At the same time, the lower Ca content means that less CaO could react with the solid Al₂O₃ inclusions to form liquid inclusions [7]. Also, previous heat can leave slag remains on the ladle walls [21]. In the present experiments, the ladles had previously been used 68, 6 and 18 times for heat 1, 2 and 3, respectively. In heats 1 and 3 the amounts of inclusions originating from the slag were 71% and 73% of the total amount inclusions, respectively (Table 6) . The corresponding amount of inclusions from heat 2 of inclusions originating from the slag was 39%. Thus, these results indicate that when the ladles are reused at least 18 times this will increase the risk of carryover of slag remains from previous castings [21].

The inclusions that are solid and contain a high AI_2O_3

Table 2. Chemical composition of the slag, wt-%

Component	MgO	CaO	Al ₂ O ₃	SiO ₂	FeO	%CaO/ %SiO ₂
Ladle slag - H1	9.8	58.4	24.7	4.7	0.008	12.4
Ladle slag - H2	9.0	58.2	24.9	5.4	0.006	10.8
Ladle slag - H3	8.9	59.5	24.1	5.1	0.005	11.7

Table 3. Chemical composition of the steel melt in heat 1, wt-%

Component	Al	Ca	Si	Mn	Мо
VDS	0.058	0.0009	0.214	1.254	0.607
MA1	0.054	0.0008	0.220	1.256	0.608
MA2	0.054	0.0008	0.218	1.249	0.606
MB1	0.055	0.0009	0.219	1.255	0.611
MB2	0.058	0.0010	0.222	1.260	0.606
MC1	0.057	0.0010	0.218	1.254	0.610
MC2	0.057	0.0008	0.218	1.249	0.607

Table 4. Chemical composition of the steel melt in heat 2, wt-%

Component	Al	Ca	Si	Mn	Мо
VDS	0.052	0.0006	0.205	1.268	0.604
MA1	0.046	0.001	0.208	1.270	0.600
MA2	0.045	0.0006	0.205	1.262	0.603
MB1	0.044	0.0005	0.204	1.261	0.600
MB2	0.046	0.0005	0.201	1.251	0.600
MC1	0.050	0.0008	0.207	1.261	0.596
MC2	-	-	-	-	-

Table 5. Chemical composition of the steel melt in heat 3, wt-%

Component	Al	Ca	Si	Mn	Мо
VDS	0.060	0.0014	0.226	1.224	0.621
MA1	0.047	0.0008	0.213	1.218	0.619
MA2	0.046	0.0008	0.213	1.220	0.617
MB1	0.049	0.001	0.213	1.228	0.620
MB2	0.048	0.0009	0.212	1.216	0.612
MC1	0.050	0.0009	0.213	1.219	0.615
MC2	0.064	0.0013	0.224	1.234	0.604

Table 6. Amount of inclusion in the slab

Heat	1, DM	1, DL	2, DM	2, DL	3, DM	3, DL
Group I	73%	50%	36%	57%	81%	40%
Group II	0%	0%	38%	29%	3%	0%
Group III	20%	50%	19%	14%	5%	0%
Group IV	7%	0%	6%	0%	11%	60%
n	15	2	47	7	37	5
NA	3.9E-02	5.2E-03	1.2E-01	1.8E-02	8.0E-02	1.1E-02
A [mm ²]	387	387	400	400	466	466
ντ 1 '	· d	0 0000				

*Inclusions with >60 wt% CaO

content around 60-100 wt-% are deoxidation products, as seen in Figure 5. It is of most importance that these harmful inclusions are separated to the tundish slag ^[6]. If these inclusions are not removed, they may cause clogging of the submerged entry nozzle. Here, the calcium treatment in the ladle is important, since a reaction between CaO and Al₂O₃ will form calcium aluminate inclusions. These inclusions are liquid at steelmaking temperatures. Therefore, they have a smaller tendency to form clusters as well as a smaller tendency to cause clogging of the submerged entry nozzle [7]. From the steel composition for all heats in Tables 3-5 it can be seen that the amounts of Ca and Al in the steel melt are generally lower in heat 2 compared to in heats 1 and 3. However, the origin of the inclusions cannot be determined precisely since inclusions also can react with the molten steel [21]. The steel grade in all heats was killed with aluminium as well as calcium treated. Inclusions with a composition similar to those elements can be formed by the slag [21]. Therefore, this will result in an increased amount of deoxidation products



SEM – Mag: 15.00 K X





Figure 5. Inclusion from MISS sample at time A in position 1, heat 3.

(Al₂O₃) and slag (calcium aluminate) inclusions as seen in the ternary phase diagrams in Figures 3-4. In heat 2 the origin of the inclusions was both slag and deoxidation products. This differed from the other heats, where almost no inclusions originated from the deoxidation products, see Table 6. It has been indicated that a higher basicity of the slag in the casting mold will increase the absorption of Al₂O₃ inclusions ^[6]. The calculated slag composition in the ladle during the VDS treatment shows that the slag in heat 2 had the lowest basicity (as %CaO/%SiO₂ ratio, 10.8) , as seen in Table 2. Heat 1 had the highest basicity (as %CaO/%SiO₂ ratio, 12.4) and no nonmetallic inclusions originating from deoxidation products were observed in this heat (Table 6) .

From Tables 1-2 it can be seen that the MgO content is the second highest in the bulk cover powder (35 wt-%) and the highest in the tundish lining refractory (60-65 wt-%). The Mg content in the molten steel is low. Thus, inclusions with contents higher than the bulk cover powder originate from the refractory lining material. In **Figure 6**, an inclusion originating from the refractory is shown. The inclusion is irregular and contains a high amount of MgO. As can be seen, a layer of calcium aluminate has started to be formed around the MgO particle ^[13]. Liquid inclusions will more easily agglomerate to semi-liquid inclusions than to liquid inclusions ^[13]. For these reasons it could be





Figure 6. Inclusion from MISS sample at time B in position 1, heat 3.

Al

assumed that inclusions with an MgO amount \ge 35 wt-% will originate from the refractory lining material. In the slab after casting, DM inclusions with an MgO content \ge 35 wt-% were also found in all the heats. Moreover, DL inclusions were found in the slabs, but in general with MgO contents \le 35 wt-%. The DL inclusions' compositions are closer to the slag composition and deoxidation products compositions. It is also known that the MgAl₂O₄ spinel inclusion will decrease the Mg content during the casting process ^[22]. This in combination with that calcium aluminate react with the MgO inclusion could explain why the overall inclusion compositions decrease from the VDS treatment, through the MISS samples in the tundish, and to the slab, as seen in Figures 3-4.

In Table 6, the percentages of the inclusion group from each heat are presented. Specifically, the four detected groups were the following: slag (I), deoxidation products (II) , refractory (III) and other (IV) . Group IV consists of inclusions that contain either a high amount of CaO (over 90 wt-%) or modified inclusions from groups I and II. In heat 1, the steel is cleanest and the sample contains 17 inclusions. For heats 1 and 3, the highest amounts of inclusions originate from the slag. In heat 3, three of 5 DL inclusions are almost pure CaO inclusions. However, this is most likely due to the calcium treatment and is not a general tendency for the 42 inclusions. In heat 2, the slag and deoxidation products were the dominating origins of the inclusions. Overall, heat 2 contained the largest amount of inclusions; i.e. 0.135 inclusions/ mm² compared to 0.044 and 0.090 inclusions/mm² for heats 1 and 3, respectively.

4. Concluding Discussion

One vital factor to reduce clogging of the SEN during continuous casting is to produce clean steels before casting. Since the tundish is the last process step where it is possible to separate non-metallic inclusions from the steel to the slag, it is important to understand the mechanisms for this separation in order be able to produce clean steel. Therefore, sampling with MISS samplers at the interface of the top layer in the tundish was carried out for three heats in order to be able to study the region close to the steel/slag interface. The steel flow inside the tundish is turbulent; after the steel hits the impact pad it will deflect in all directions that will results in recirculation loops directed towards the submerged entry nozzle [5,16,23]. Additionally, previously published results from mathematical modelling has suggested that the slag is pulled down by the down-flow of the steel flow and also that slag particles are being transported away from the inlet, along the slag/metal interface [11]. In addition, it has been reported that the upwardly directed steel flow along the sidewalls can push away the slag and therefore the concentration of the slag mass can be low [16]. In the MISS samples from positions 1 and 2 (Figure 1b) the amount of slag was found to be low. Also, since inclusions from group III were found in samples from both positions the steel flow was turbulent and interactions between the tundish cover powder slag, the molten steel and refractory can be detected in both positions 1 and 2. In addition, inclusions containing slag were found in almost all the samples. This can be explained by that the focus of the sampling was the slag/steel interface, and inclusions can "remain" in the interface before being separated to the slag. The elements used in the steelmaking process are the same elements that originate from the slag. Also, the steel flow will both drag down slag particles from the tundish slag layer into the tundish and fragments from the refractory lining. Therefore, these samples were expected to contain inclusions originating from the slag. In addition, the source that overall dominated the origin of the inclusions was the slag, as seen in Table 6. Thus, the results of this study show that the formation of inclusions from the slag is the dominating source of inclusions during casting. Moreover, it was found that this inclusion type increased with an increased ladle age.

5. Conclusion

The focus in this study was the inclusion characteristics at the steel/slag interface in a tundish during casting. Thus, the MISS sampler was implemented during one sequence casting in order to sample steel close to the steel/slag interface. Thereafter, the size and composition of the inclusions in the samples were determined by using SEM in combination with EDS. The inclusions were found to originate from the slag (I), deoxidation products (II), the refractory lining material (III) , and other sources (IV) . The more specific conclusions from this study may be summarized as follows:

- The MISS samples were collected from two positions in the tundish and there were no general differences between the two sampling positions with respect to the amount of inclusions. Overall, inclusions originating from the slag (I) were the major source in all heats. Furthermore, in heat 2 inclusions originating from the deoxidation products (II) were also common.
- Particles from the tundish refractory lining ended up in the molten steel and slab. Inclusions originating from the refractory material were found in the slab for all the three heats.
- In the heats where the ladles had previously been used 68 (heat 1) and 18 (heat 3) times before the casting, over 70 % of the inclusions originated from the slag.

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1. 緒言

鉄鋼製品の品質向上に対する要求は高まり続けており, 鋼の清浄度および製品特性の絶え間ない改善は必然となっ ている^[1,2]。鋼の製造工程の中でタンディッシュは鋳造前 の最終工程であり,そのため鋼の清浄度に対し影響を及ぼ し得る。タンディッシュの中では合金の添加や溶鋼過熱度 (Superheat)の調整,また溶鋼全体の均熱化などといった 冶金的操作が実施される^[3]。それと同時に,非金属介在物(以 降,介在物)をスラグ相へと除去できる最終工程でもある ^[3-5]。また,溶鋼の再酸化を防ぐことでも鋼の清浄度を改善 することができる^[4-5]。

介在物のスラグ相への除去が不十分であると介在物が鋼 中に取り込まれスラブの品質低下を招いてしまう^[6]ことに 加え,浸漬ノズル内面に堆積,ノズル閉塞を引き起こし,鋳造 安定性の妨げにもなってしまう^[7]。この点において,ノズル 内面付着物の組成は,タンディッシュ内に存在する溶鋼中 の介在物組成と関連があることが報告されている^[8]。

タンディッシュ内での溶鋼-スラグ-介在物という系にお いて、それぞれの界面現象が介在物のスラグ相への分離挙動 に影響することが知られている。つまり介在物の分離現 象は、溶鋼/スラグ界面での介在物の動きやスラグの粘性、濡 れ性によって影響を受ける
^[9]。さらに介在物の溶鋼からス ラグ中への除去には,密度の不規則性,乱流変動,そして溶鋼 とタンディッシュパウダー /耐火物との成分授受といった 要因が影響するため,非常に複雑なプロセスと言える[10,11]。 介在物がスラグ/メタル界面に到達したとき,その介在物は i) 界面を通過し直ちにスラグ相へ取り込まれる,ii) 界面に 留まり他の介在物と凝集し,再び溶鋼中へ戻される,または iii) 界面直下で振動し,再度溶鋼流動とともに流され製品の 欠陥となる^[4]。また,介在物の大きさが150~180µmの場 合は,スラグ中へ取り込まれた介在物の周りには薄い溶鋼の フィルムが生成されることも報告されており,この現象によ るスラグへの介在物吸収に対する影響も考えられる[4,12]。

介在物が溶鋼/スラグ界面に到達したとしても,不安定さ や乱流の変動により,スラグ中へ取り込まれる前に界面に 滞在することもある^[10,11]。さらに,小径の介在物は乱流に より凝集・大型化し,溶鋼からの除去が容易となる^[5]。しか しながら介在物の凝集挙動は,介在物が溶鋼/スラグ界面に 存在するときよりもスラグ中に存在する方が促進されると 報告されている^[13]。介在物のスラグ相への除去を最大限実 施するためには,系全体(溶鋼/スラグ/介在物界面)の高い 濡れ性と,スラグ巻き込みが生じない範囲での低いスラグ の粘性が必要と言われている^[4,12]。しかしながら,スラグ中 へのAl₂O₃介在物の吸収はスラグ組成を変動させ,これはス ラグの粘性を変化させることが知られている^[14]。またタン ディッシュ内でのスラグ組成は,取鍋からのカルシウムア ルミネート系スラグの流入によっても影響を受ける^[15]。タ ンディッシュ内のスラグは鋳造条件によっては溶鋼へと巻き込まれ、これは新しい介在物を生成する^[10,11]。具体的には、たとえ水平方向かつ低速度のスラグ流動であったとしても、溶融スラグがちぎ取られ介在物として分散してしまうことがある^[11]。また、タンディッシュ内の溶鋼流動解析結果から、溶鋼のスラグ中への巻き込み、またその逆のスラグの溶鋼中への巻き込み挙動は溶鋼の循環流も影響していることが示されている^[16]。さらに、溶鋼流動によって相当数の介在物がタンディッシュ内部や下部に流され、このことにより介在物の除去が妨げられることも報告されている^[16]。

タンディッシュ内の溶鋼は雰囲気やタンディッシュスラ グ,耐火物からの酸素供給によって再酸化され得る。この 現象は最終製品の清浄度に影響を及ぼす^[2,10,17]。タンディッ シュ内で使用される耐火物はMgO基であり,Fayalite (Fe₂SiO₄) とForsterite (Mg₂SiO₄)の固溶体である Olivineで構成されている^[17]。このMgO基の耐火物は,低級 酸化物濃度が低いことから耐火物として安定な材料である ことが示されているが^[17],Olivineはアルミキルド鋼と下に 示す(1),(3),(5)の反応を生じ得る^[17]:

$2Fe + 2O + SiO_2 = Fe_2SiO_4$	(1)
$\Delta G^{0}_{f} = 1379.93 \text{ [kJ/mole]} (298.15 \text{ K})^{[18]}$	(2)
$Mg_{2}SiO_{4} + SiO_{2} = 2MgSiO_{3}$ $\Delta G^{0}_{f} = 3301.44 \text{ [kJ/mole]} (298.15 \text{ K})^{[18]}$	(3) (4)

 $MgO + Al_2O_3 = MgAl_2O_4$ (5) $\Delta G^0_f = -2188.96 \text{ [kJ/mole]} (298.15 \text{ K})^{[18]}$ (6)

溶鋼が耐火物ライニングに浸潤すると,溶鋼中に存在す るアルミニウムとの反応によって溶鋼/耐火物界面にスピ ネル粒子が生成される^[1]。同時に,これらの粒子は耐火物か ら溶鋼中へと遊離し,溶鋼/耐火物近傍における介在物とな り得る^[1,17]。これらの介在物は共通して内部にシリケート 系やMgO単相を含有する^[1]。耐火物材料中と溶鋼中での酸 素ポテンシャルの違いから,溶鋼/耐火物界面には酸化鉄の 層が形成されることも報告されており^[1]また,耐火物中に内 在する空隙中の空気や耐火物中に含まれる低級酸化物もこ の酸素供給源となり得る^[1]。シリケート系の酸化物は,これ ら酸化鉄層の中に含まれる全ての酸化物を溶かす^[1]ため,そ の結果Al₂O₃やCaO,FeO,MgO,そしてSiO₂を含む複雑な組 成を持つスラグが生成されることとなる^[1]。

タンディッシュ耐火物およびタンディッシュスラグの両 方が,溶鋼中に存在する介在物の起源,または組成変化の要 因となり得る^[2,10]。それゆえ,清浄度の高い鋼を製造するに は,耐火物/溶鋼間および溶鋼/スラグ間での起こり得る反応 を理解することが重要となる^[4]。実際は,物理モデリングお よび数値解析モデリングとフルスケールシステムとの違い により,溶鋼からスラグへの介在物除去挙動を正確に表現 することは未だ難しい^[3]。

タンディッシュ内での介在物挙動に関する本研究は,解 析ではなく実験的であり,実際の製造工程内にて実施され たものである。実験では様々な介在物の挙動を研究すべく, タンディッシュ内において平行の位置関係にある二か所か ら溶鋼/スラグ界面のサンプルを数回採取した。さらに,溶 鋼/スラグ界面や溶鋼/耐火物界面,また種々の反応がどのよ うに介在物の大きさや組成に影響するかについて焦点を当 て調査を実施した。

2. 実験方法

2.1. 溶鋼/スラグ界面サンプルの採取

実機における本調査はスウェーデンOxelösundに位置 し,高炉ー貫製鉄所であるSSABにて実施した。当工場は軽 量高機能鋼から過酷な環境下で使用される大型鋼材までの 幅広い範囲の高強度・構造用鋼を製造している。SSABの 製造工程は高炉から始まり,トーピードカーにて溶銑を脱 硫し,転炉で脱炭を実施することで鋼を製造し,次いで取鍋 精錬にて合金の添加と水素,硫黄,酸素を除去し,最終的にス ラブへと鋳造する工程である。

本実験は構造用鋼(0.165% C, 0.055% AI, 1.25% Mn, 0.22% Si, 0.6% Mo, 0.2 % Cr, wt-%)の製造プロ セスにおいて実施した。取鍋精錬の鍋容量は190tであり, 脱酸剤としてはアルミニウムを用い,また介在物形態制御を 目的としてカルシウムを使用した。精錬を終えた取鍋は鋳 造機へと運ばれ,容量30tのタンディッシュを用いて鋳造し た。スラブの寸法は220×1680mmである。タンディッシュ のライニング,および各パウダー組成をTable 1に示す。

スラグと溶鋼との相互影響を調査するため,試料採取に はMISS (Momentary Interfacial Solidification Sampling ^[10,19]) サンプラーを使用した。本MISSサンプラーは12mm 厚さの鋼板にて作製され,内部に鋳型(120×100mm)形 状を形成するべく二枚が溶接されており,80×8mmの棒が 取り付けられている。Figure 1aに採取したサンプルを示 しており,同図には試料切り出し・分析部位も記している。 MISSサンプラーは採取後に試料が再加熱されないように ウールにより断熱されており,また内面は試料との濡れ性 向上のためにエッチング処理を施している。このMISSサン プラーを用いることで溶鋼/スラグ界面の試料を採取し^[11], 本試料に対しFEG-SEM (Zeiss Merlin,Oxford Instruments INCA Feature for Windows 7付) とEDS (Energy Dispersive Spectrometer)を組み合わせ使用することで 調査を行った。

各ヒート毎6つのMISSサンプラーを使用し,順次その次の試験に再使用することで合計3ヒートについて調査を行った。サンプルは鋳造開始初期(試料MA1,MA2),溶

鋼をおおよそ半分鋳造した時(試料MB1,MB2)そして鋳 造を終了し次ヒートの鋳造へ移行している時(MC1,MC2) においてそれぞれ採取した。試料の採取はMISSサンプラー をタンディッシュ内に浸漬させ5秒保持することで行っ た。タンディッシュ内における溶鋼/スラグ/耐火物相互影 響を詳細に調査すべく,試料採取場所は操業上立ち入りが 容易な場所から二か所の,互いに平行する場所を選んだ。 一つ目のサンプリング場所は耐火物壁の近傍(壁から 110-150mmの位置)とし,これは耐火物ライニングに起 因した介在物有無の調査を目的とした。二つ目のサンプリ ング場所は耐火物壁から離れ,おおよそタンディッシュの 中央に位置しており,主にタンディッシュパウダーと溶鋼 との相互影響を調査することを目的とした。

これら二つの試料採取位置をFigure 1bに示す。これら タンディッシュからの試料採取に加え、各ヒート毎に1試料 (ロリポップ方式、12mm厚)を鋳造の前工程であるVDS (Vacuum Degassing Station)脱ガス工程終了後に取鍋 より採取した。また各ヒート鋳造後のスラブにおいても、 スラブ表面から1/4深さのところから試料を1つ採取し研 究に供した。スラブからの試料採取条件としては、鋳造定 常状態での品質を得るべく取鍋内の溶鋼を約半分鋳込み終 えたときのスラブを選んだ。

2.2. タンディッシュから採取した試料の分析方法

MISSにより採取したサンプルを用い、中央上部の位置 (Figure 1a,領域1)より1試料を切り出した。試料の大き さは20×30mmとし、ベークライトに埋め込んだのちに研 磨,洗浄した。介在物の組成や形態,円相当径(ECD: Equivalent Circle Diameter)の調査はINCA Feature付 FEG-SEMとEDSを組み合わせて使用することで行った。 INCA Featureによる調査はECDが5.7µmよりも大きい介 在物を対象とし、介在物を検出後手動調査することでエラー (穴やダスト)を排除した。VDS後およびスラブから採取 した試料についても同様の調査を実施した。また,鋼中成分 の分析はOES (Optical Emission Spectrometry)を用いた。

INCA Featureによる調査結果から,本研究における介在 物はその大きさから二つのグループに分けられることが分 かり,一方をDM介在物(ECD 5.7-11.2 µm),もう一方を DL介在物(ECD ≥11.3 µm)と定義した。

3. 結果および考察

MISSサンプラーを用いた過去の研究では,僅かに凸形状 を呈したスラグ表面層が試料上部に得られていた^[11]。本研 究では,タンディッシュスラグ相は①溶鋼と接触し反応性 のある溶融スラグ層と②溶融しない断熱層との2層構造と なっていると考えていた。しかしながら,本MISS試料では この溶融スラグ層を観察することが困難であった。従って, 顕微鏡調査はMISS試料中,溶鋼/スラグ界面近傍に位置した介在物を対象とした。

INCA Featureによる調査結果は,介在物組成分析結果を 鑑みAl₂O₃,CaO,MgO三元系にノーマライズした。これは、 上記3つの成分がその他の成分よりも著しく高かったため である。Al₂O₃-CaO-MgO 三元系状態図をFigure 2に示 す[20]。介在物調査結果はヒート毎,各サンプリング時期に ついてプロットした ((a): VDS後, (b): 鋳造開始初期, (c) :鋳造中期,(d):鋳造終了時,(e):スラブ)。Figure 3,Figure 4にヒート2,ヒート3の介在物調査結果を示す。ヒート1の 結果はヒート3の結果と似ていたため図示は省略した。図 より,介在物はその起源を(I)スラグ,(II) 脱酸生成物,(III) 耐火物の3つのグループに分類できることが分かる。スラ グに起因した介在物(I)は,鋳造温度である1522-1541 ℃において液体領域に組成が位置している。溶鋼中のアル ミニウムはO2と反応することでAl2O3介在物を生成するこ とから,脱酸生成物を起源とした介在物(II)は60-100wt-%のAl₂O₃を含む。3つ目のグループ(III)に分けられる介 在物は高MgO組成であり,これはタンディッシュのライニ ング材に起因している。

計算により求めた取鍋スラグ組成をTable 2に示す。ス ラグ組成は前述した三元系状態図中の液相領域近傍に位置 している (Figure 2)。スラグに起因した介在物の組成は この液体領域組成に位置し,そしてそれらのMgO濃度は低 く10wt-%未満であった。全ヒートにおいて,スラブ試料 からはこのスラグ起因介在物が多く検出され,またスラグ 起因介在物はDM介在物とDL介在物の両方から検出され た。しかしながら、ヒート1、ヒート3ではこれらスラグ起因 の介在物が主要な介在物でありCaO濃度は40-60wt-%程 度であったのに対し,ヒート2では比較的CaO濃度が低く, 概して40wt-%未満であった(Table 3-5)。ヒート2では 鋳造中期に採取したサンプル中のCa濃度が0.0005wt-% であり,これは同時期に採取した他ヒートの試料の約半分 の濃度であった。つまりヒート2における介在物中の低い CaO濃度(Figure 3)は、溶鋼中の低いCa濃度(Table 4) と良く対応していることとなる。さらに、溶鋼中のCa濃度 が低いことは,液体介在物を生成する反応である固体Al2O3 介在物とCaOとの反応量も少ないことを意味する^[7]。また, 取鍋が受鋼した前ヒートのスラグは取鍋壁に残存し得る[21] と言われており,本研究ではヒート1,2,3の取鍋は実験まで にそれぞれ68回,6回,18回の溶鋼を処理していた。ヒート 1および3では、検出された介在物のうちそれぞれ71%、 73%をスラグ起因介在物が占めていた(Table 6)一方で, ヒート2においてこれに該当する介在物は39%であった。 すなわち本研究の結果からは、取鍋を18回以上使用するこ とにより前ヒートからのスラグの持ち越しの可能性が高ま ることが示唆された[21]。

Figure 5に見られたように,固体状態かつ60-100wt-%

といった高いAl₂O₃濃度を有する介在物は脱酸生成物であ ると考えられる。これら介在物は浸漬ノズルの閉塞を引き 起こすため,タンディッシュスラグへと除去されるべきで ある^[6]。同様に,カルシウム処理を施すことでCaOとAl₂O₃ とを反応させ,製鋼温度域において液体状態の介在物へと 改質することも重要となる。これら液体状態の介在物はク ラスター形成の可能性を低減させるだけでなく,浸漬ノズ ル閉塞のリスクも低減させることとなる¹⁷。Table 3-5に 示した鋼中成分分析結果から,ヒート2におけるCaおよび Al濃度はその他ヒート1,3よりも全体的に低いことが見て とれる。しかしながら介在物は溶鋼とも反応するために介 在物の起源を正確に判定することは困難ではある[21]。本実 験の全てのヒートはアルニミウムにより脱酸されており, またカルシウム処理も施されている。また,これらの成分 を含んだ介在物はスラグによっても生成され得る[21]。すな わち,これらアルミニウムによる脱酸操作およびスラグの 存在は,Figure 3およびFigure 4にて確認された脱酸生成 物であるAl₂O₃介在物とスラグ起因介在物(カルシウムア ルミネート)の両方の生成に繋がる。

Table 6に示したようにヒート2においては介在物の起源はスラグと脱酸生成物の両方であり,対してその他の ヒートでは脱酸生成物に起因した介在物はほとんど検出されなかった。これまでの研究で,モールド内のスラグが高塩基度であるほどAl₂O₃介在物のスラグへの吸収が促進されることが報告されている⁽⁶⁾。この点において,Table 2に示したVDS処理中の計算スラグ組成から,ヒート2のスラグが最も低塩基度であったことが分かる(%CaO/%SiO₂ = 10.8)。対してヒート1,3ではスラグ塩基度は高く(%CaO/%SiO₂ = 12.4),これらのヒートでは脱酸生成物起因の介在物は検出されていない(Table 6)。

Table 1, Table 2から, 最も高MgO濃度の部位はタン ディッシュライニング耐火物であり(60-65wt-%),次い でバルクカバーパウダーであることが分かる(35wt-%)。 溶鋼中のMg濃度は低いことから,従ってバルクカバーパウ ダーよりも高いMgO濃度を有する介在物は耐火物起因で あると判断できる。Figure 6に耐火物起因介在物の調査結 果を示す。介在物の形状はその他の介在物と比べ歪で凹凸 があり、そして高いMgO濃度を有している。そして同図で 確認できるように、当該介在物の周囲ではカルシウムアル ミネート相の生成が始まっていることが分かる[13]。これま での研究より,液体介在物は液体介在物同士よりも固-液共 存介在物との方が凝集し易いと言われている[13]。つまりこ の介在物同士の凝集挙動によって,MgO濃度を35wt-%以上含む耐火物起因の介在物が生成されたと推察され る。全てのヒートで,MgO濃度を35wt-%以上含む介在物 はDM介在物としても検出された一方で,スラブ中に検出さ れたDL介在物のMgO濃度は概して35wt-%以下であり、そ れらの組成はスラグ組成もしくは脱酸生成物組成に近かつ

た。MgAl₂O₄スピネル介在物中のMg濃度は鋳造時に低下 するという先行研究結果^[22]および,カルシウムアルミネー ト介在物とMgO介在物との溶鋼内反応も起こること考え られることから,これらの要因が本研究におけるVDS処理-タンディッシュ-スラブ間での介在物中Mg濃度の低下に 寄与したと推察される。

介在物を(I) スラグ,(II) 脱酸生成物,(III) 耐火物,(IV) その他のグループに分類し,それぞれの検出割合をヒート毎 にTable 6に示した。その他グループ(IV) に分類された介 在物については高CaO含有介在物(90wt-%以上)を含ん でいる。本調査結果ではヒート1が最も清浄度が高く,介在 物の検出個数は17個であった。また,ヒート1とヒート3は 共通して,介在物はスラグ起因のものがほとんどであった。 ヒート3においてはDL介在物が5つ検出されたがそれらは ほぼ純CaO組成の介在物であり,これはカルシウム処理に起 因するため,当ヒートで検出された全42個の介在物の傾向 を示すものでは無いと考えられた。ヒート2ではスラグお よび脱酸生成物が介在物のほとんどを占めており,調査した ヒート中最も介在物の検出頻度が高かった(ヒート1:0.044 個/mm²,ヒート2:0.135個/mm²,ヒート3:0.090個/mm²)。

4. 考察まとめ

連続鋳造における浸漬ノズル閉塞を防止するための一つ の有効な手段は清浄度の高い鋼を溶製することである。タ ンディッシュは介在物をスラグ中へと分離できる最終プロ セスであることから,高清浄度鋼製造を実現するには当プ ロセスでの介在物除去メカニズムを理解することが重要と なる。そのため本研究では合計3ヒートの製造プロセスを 対象とし,MISSサンプラーを用いてタンディッシュ内溶鋼 /スラグ界面の試料を採取し研究を行った。

タンディッシュ内での溶鋼流動は乱流であり,取鍋から タンディッシュへの注入流がインパクトパッドに衝突した 後,溶鋼は様々な方向へ流れを変える。これによりタン ディッシュ内では溶鋼流動の再循環ループが形成され,-部は浸漬ノズルへと向かう[5,16,23]。さらに、既報の数値シ ミュレーション結果では、溶鋼の下降流に従ってスラグが 溶鋼内に巻き込まれ,さらにこのスラグ粒子は溶鋼/スラグ 界面に沿って溶鋼流入部から遠くへ輸送され得ることが報 告されている[11]。また,タンディッシュ内側壁付近での溶 鋼の上昇流によりスラグが押し出され,スラグ量が不足す るという現象も報告されている[16]。本研究でMISSサンプ リングとして設定した場所 (Figure 1b) ではスラグ量は 少なく見受けられた。グループIII(耐火物起因)に分類さ れる介在物が本実験の二つの試料採取場所の両サンプルか ら検出されたことから,溶鋼流動は乱流状態であり,タン ディッシュカバーパウダー /溶鋼/耐火物の相互反応はどち らの採取場所においても認められたこととなる。このこと

から,介在物は除去されずに溶鋼/スラグ間に"残存"して いたと理解できる。製鋼工程において用いられている成分 はスラグに起因する成分と同様であり,また,溶鋼流動はタ ンディッシュスラグに起因したスラグ粒子,そして耐火物 の欠片の両方を下方へと流し落とす。従って,本研究で採 取したサンプルにはスラグ起因の介在物を含んでいると考 えることができる。さらに,本研究結果のTable 6に示した ように,鋳造時溶鋼中に存在している介在物のほとんどは スラグ起因であり,そしてこのタイプの介在物は取鍋の使 用回数とともに増加することが分かる。

5. 結言

本研究は連続鋳造時タンディッシュ内での,溶鋼/スラグ 界面における介在物に着目して行われた。調査方法として MISSサンプラーを採用し,溶鋼/スラグ界面のサンプルを 採取後,界面付近において検出された介在物の大きさおよ び組成をSEM/EDSにより特定した。介在物の組成は(I) スラグ,(II) 脱酸生成物,(III) 耐火物,そして(IV) その 他起因に分類された。以下に本研究の結果をまとめる。

・MISSサンプラーによりタンディッシュの二つの異なる 場所から試料を採取したが,介在物の量について差異は認 められなかった。全ヒートを通じて,スラグが介在物の主 たる起源であることが示された。ヒート2においては,スラ グ起因介在物に加えてグループIIに分類される脱酸生成物 起因の介在物も検出された。

・溶鋼内,スラブ内ともにタンディッシュ耐火物に起因する 介在物が検出され,特にスラブ内では全てのヒートでタン ディッシュ耐火物起因の介在物が認められた。

・使用回数が68回(ヒート1),18回(ヒート3)を超え た取鍋を用いたとき,鋳造時溶鋼内に存在する介在物の 70%以上はスラグ起因の介在物であった。

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一 省略 一

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